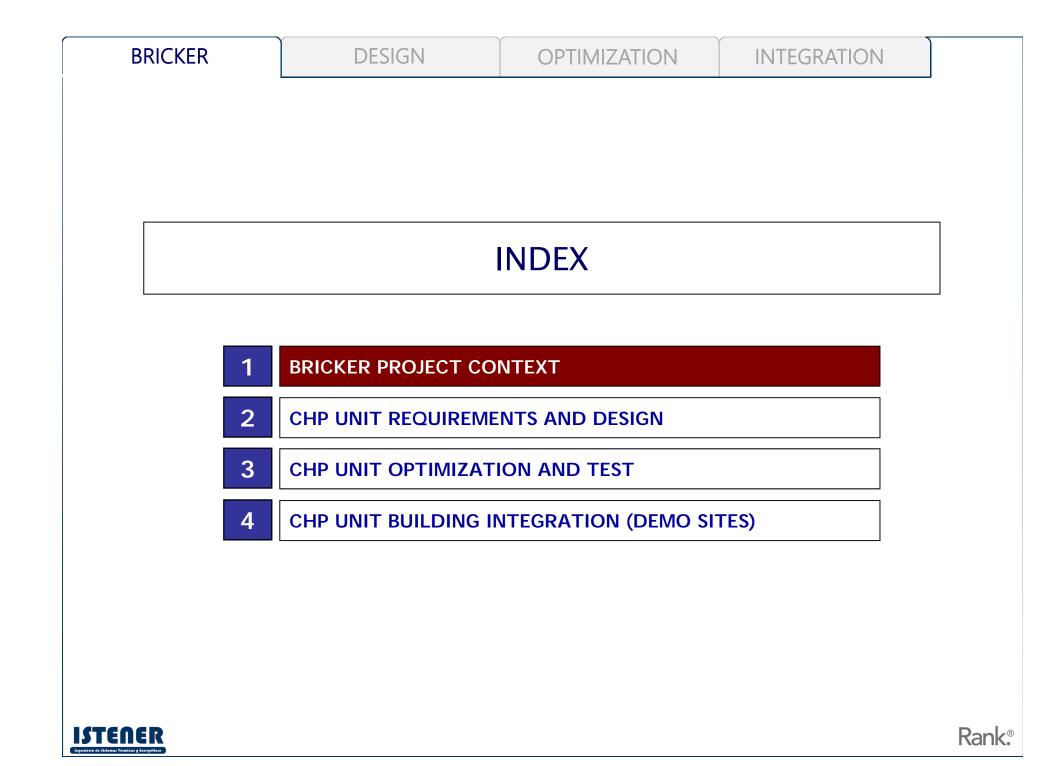




ORC based CHP unit as active technology for reducing CO2 emissions in public buildings (BRICKER Project)

Prof. Joaquín Navarro Esbrí ISTENER Research Group Director Rank® founding partner

BRICKER	DESIGN	OPTIMIZATION	INTEGRATION	
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3	CHP UNIT OPTIMIZAT	ION AND TEST		
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The global contribution from buildings towards energy consumption has steadily increased reaching near 40% in developed countries. Buildings in EU27 Member States are responsible for 40% of Europe's energy consumption and 36% of CO2 emissions.





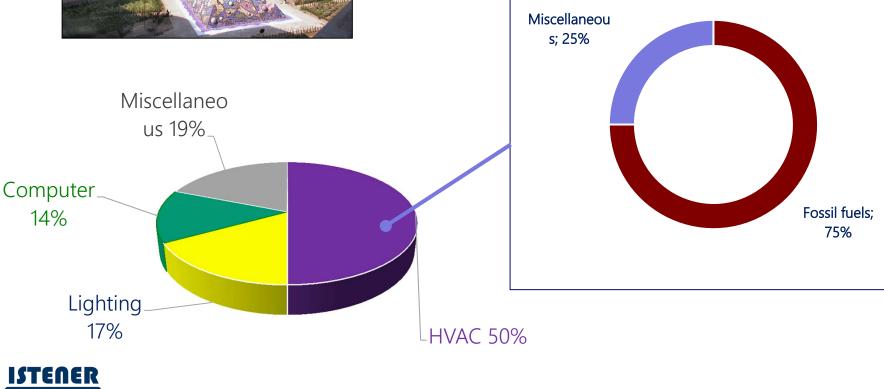


BRICKER

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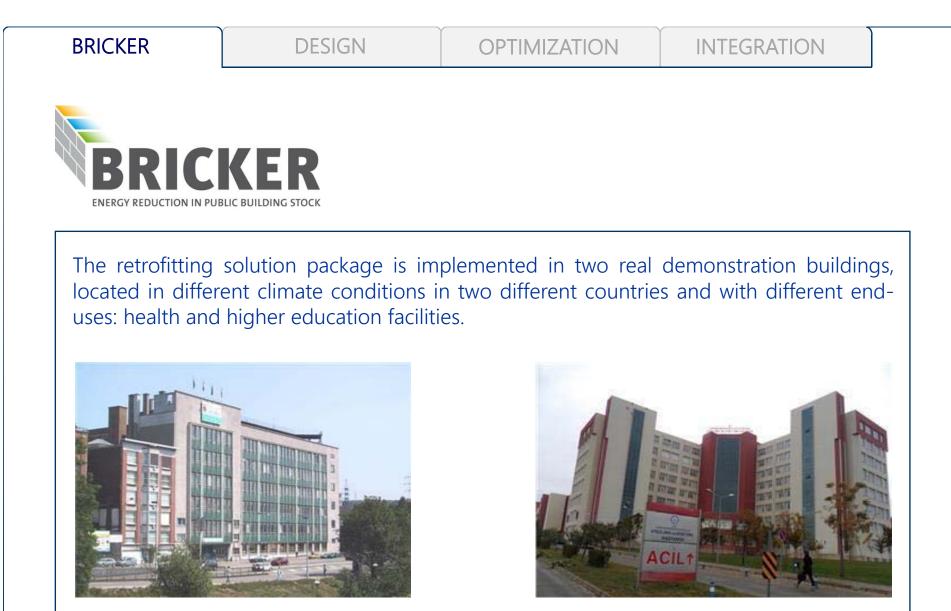


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	DESIGN	OPTIMIZATION	INTEGRATION
BRIC	KER		
ENERGY REDUCTION IN PUBL			
residential buildi	ngs in order to achiev		tisting public-owned non the energy consumption goal is achieved by:
Reducing the	building demand with	envelope retrofitting	
		nergy production tech available and clean rene	nnologies based on a ewable sources.

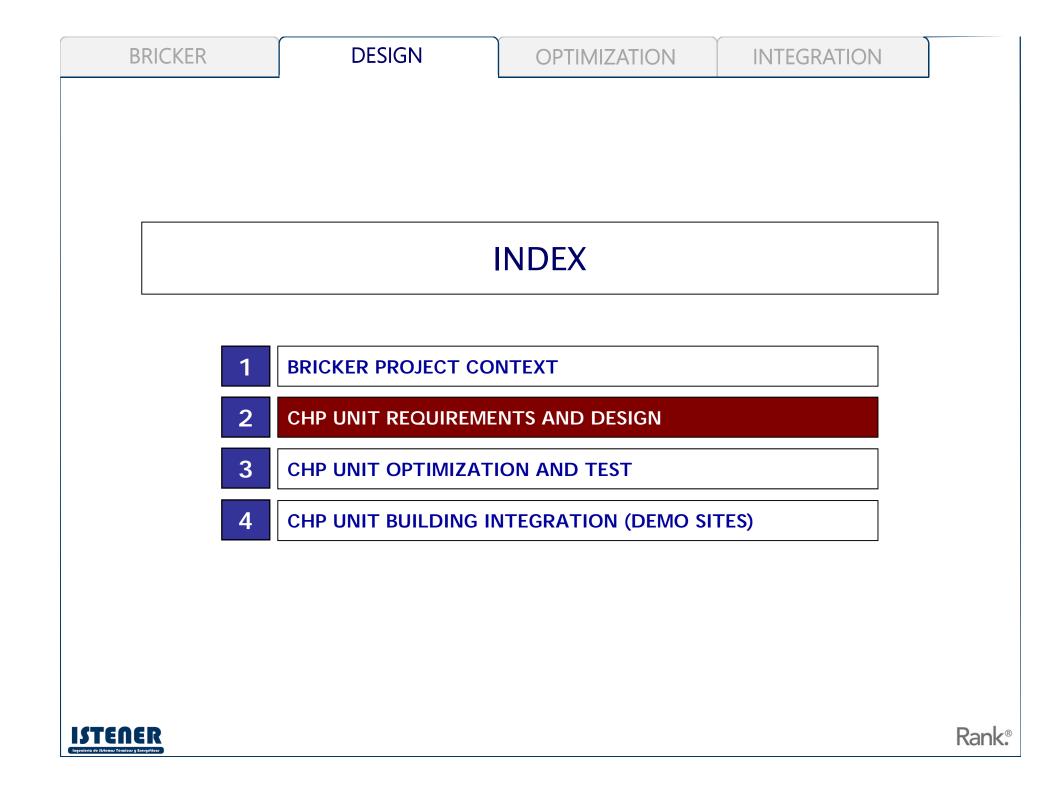




Engineering college located in Liège

University hospital located in Aydin







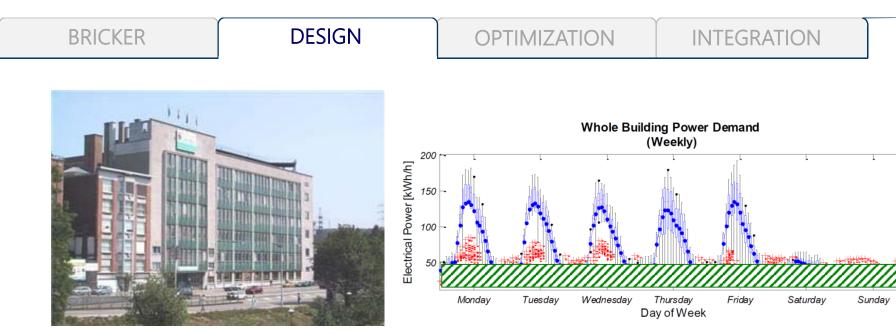
Engineering college located in Liège

Monthly heating demand (2012)

HEATING DEMAND

Month	Energy		Power [kWt]	Days with	
wonth	[kWh]		Maximum	Minimum	demand
January	407,106	2,678	6,298	1,701	16
February	424,409	2,234	3,504	1,592	20
March	352,869	1,615	2,875	1,111	23
April	214,379	1,128	2,112	368	20
Мау	109,195	500	1,621	105	23
June	0	0	0	0	0
July	0	0	0	0	0
August	0	0	0	0	0
September	122,698	615	1,224	178	21
October	221,549	1,060	2,120	221	22
November	347,054	1,661	2,952	761	22
December	333,123	2,192	3,860	1,312	16
Total	2,532,382	1,457	6,298	105	183





Engineering college located in Liège

	Average of annuities 2010, 2011 and 2012 [kWe]				
Month	Day	Night	Weekend		
January	185	98	64		
February	190	104	54		
March	177	102	55		
April	164	96	39		
Мау	166	87	88		
June	104	58	26		
July	46	27	20		
August	79	63	20		
September	155	90	36		
October	171	93	53		
November	176	98	44		
December	181	98	52		

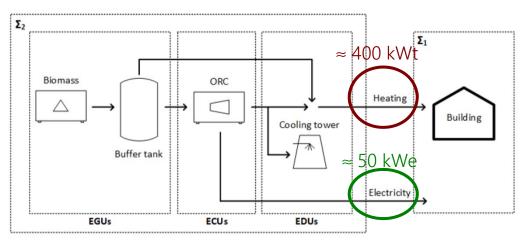
ELECTRICITY DEMAND





DESIGN





Engineering college located in Liège

TECHNICAL REQUIREMENTS

Only electricity and heating are considered.

- ORC should be activated using biomass and work as many hours as possible in best global efficiency operating point
- So, the equipment must be designed to attend the base heating demand in the form of hot water between 60 and 80°C
- The equipment must satisfy as much as possible the base of the electrical demand



BRICKER

DESIGN



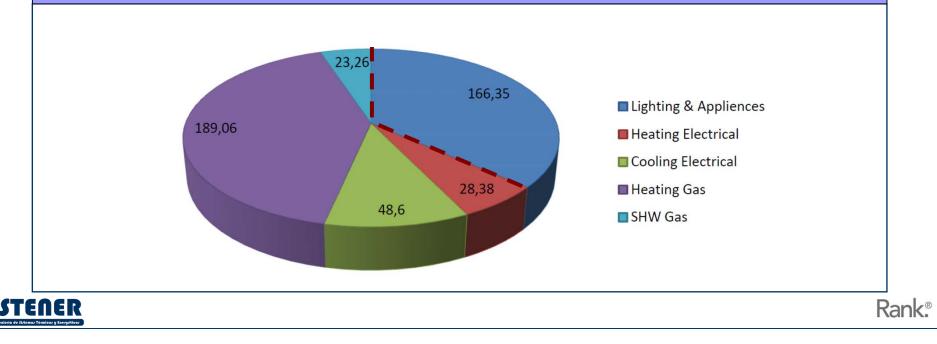
University Hospital located in Aydin

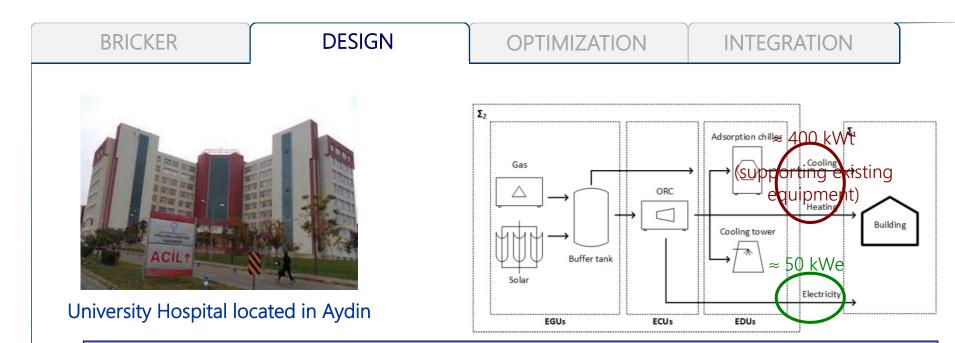
The final energy demand for heating and cooling amount to 87.4 kWh/(m2y) and 28.2 kWh/(m2y), respectively

- 13,000 kWt Natural gas boilers installed for heating and SHW
- 10,000 kWt centrifugal chiller for cooling demand

The primary energy content for heating is due to gas consumption, while for cooling is associated to electricity consumption.

ELECTRICITY, HEATING AND COOLING DEMAND





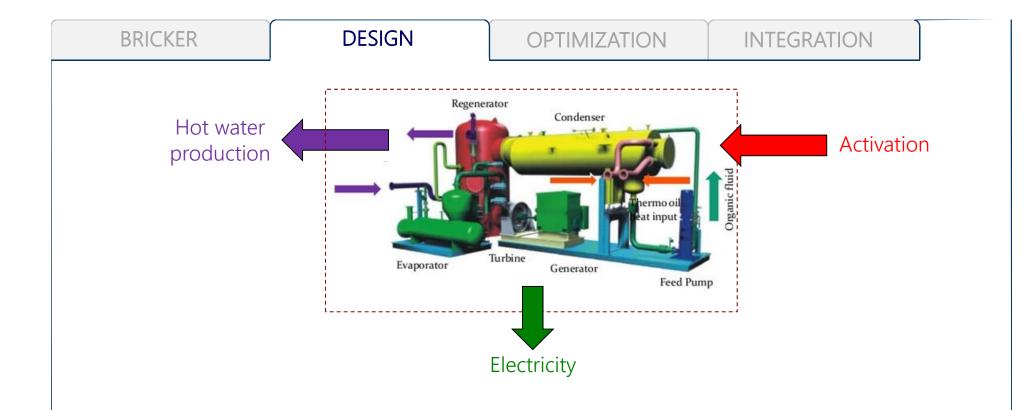
TECHNICAL REQUIREMENTS

Due to the importance of the refrigeration, it has been also included in the CHP requirements and the CHP unit will contribute to the electricity, heating and cooling demand (using and adsorption chiller).

Because of the size of the hospital building, the contribution provided by the BRICKER system will only cover a small part of the total load of the building. Therefore, the existing system and the BRICKER system will be operated jointly and the CHP unit requirements are taken from Liège.

- Due to the climate conditions, the ORC should be solar activated.
- So, being solar activated, the equipment should contribute as much as possible to the electricity, heating and refrigeration demand, depending on the power supplied by the solar collectors.

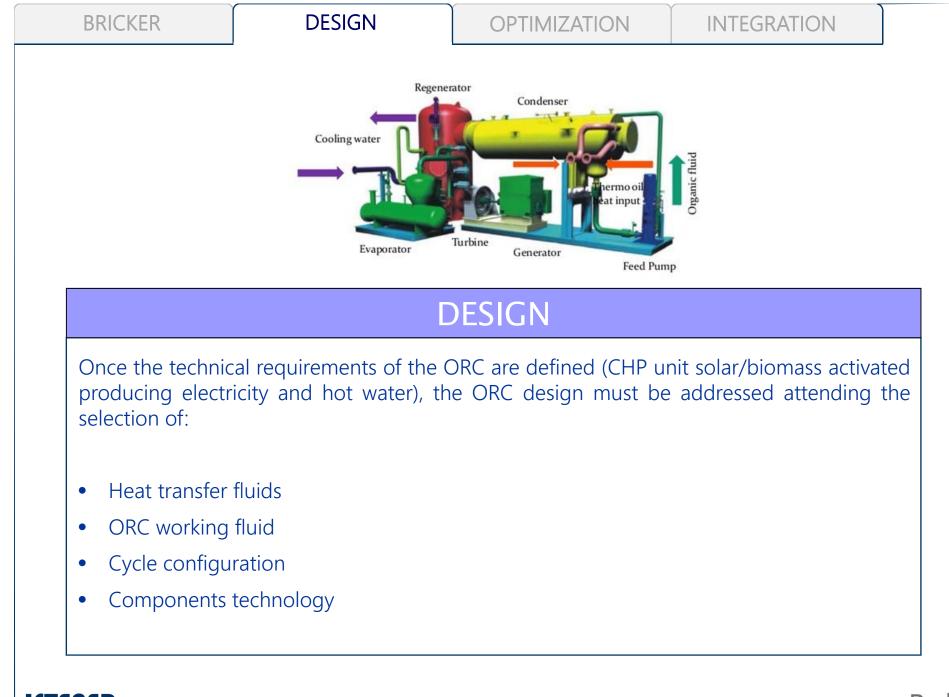




CHP TECHNICAL REQUIREMENTS

- Activation with low temperature (compatible with solar collectors technology \rightarrow about 250°C)
- Net electricity production about 50 kW (compatible with electricity consumption base in Liège)
- Hot water production between 60 and 80 °C (about 400 kW, compatible with heating consumption base in Liège)

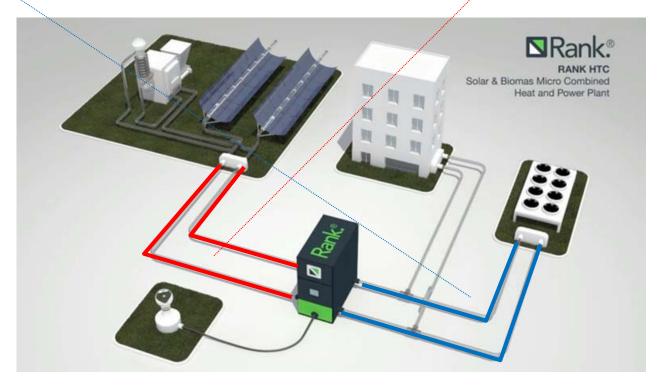




Heat transfer fluids

The heat transfer fluid selected for the activation loop has been <u>thermal oil</u>. The possibility of using steam or pressurized hot water as heat transfer fluid has been rejected.

<u>Water</u> is the fluid that is heated at the ORC condenser for attending the heating or cooling demand (through an adsorption chiller)

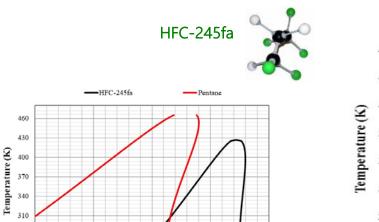




ORC working Fluid

Regarding the working fluid selection, special attention has been taken in security properties, as toxicity and flammability, thermal stability and environmental properties.

Fluid	Toxicity/Flammability	GWP	ODP	Tcrit (ºC)	Pcrit (bar)	Tmax (ºC)
Isopentane	600/Flammable	11	0			
R245fa	400/Non-flammable	950	0	154	36.51	250
R1233zd(E) - HCFO	800/Non-flammable	1	~0	165.6	35.71	200
R1336mzz(Z) - HFO	500/Non-flammable	2	0	171.3	29	250
SES36	1000/Non-flammable ^(*)	3710	0	177.55	28.49	190

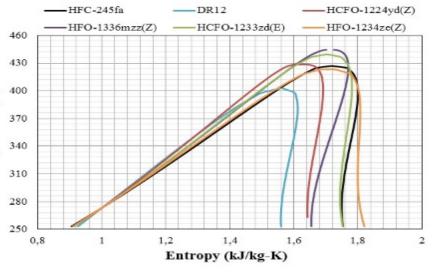


1,5

1

Entropy (kJ/kg-K)

2



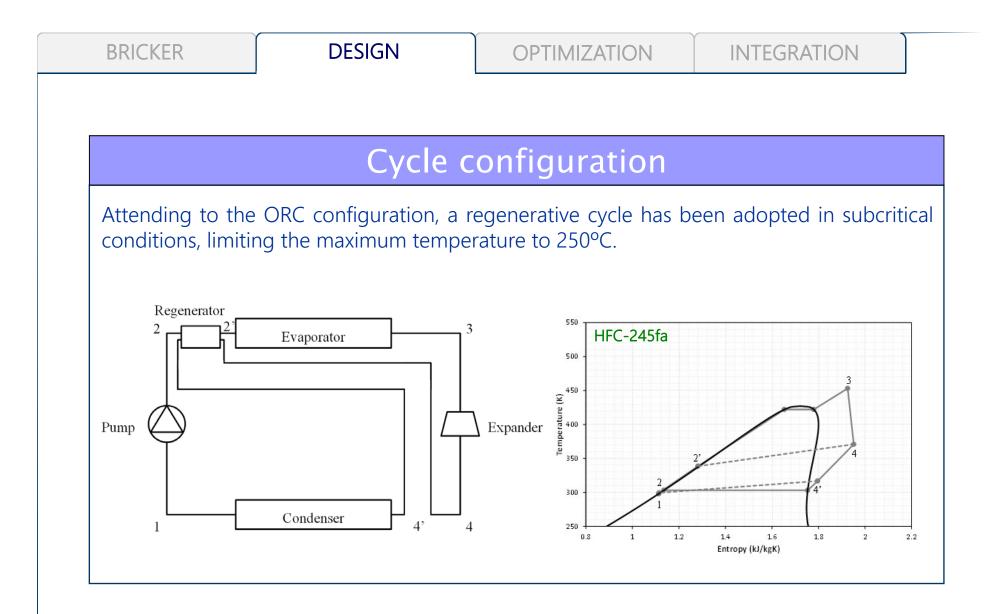


280

250

0

0.5





Components and technology adopted

- Compact brazed plate heat exchangers
- Volumetric expander
- ORC pump

ORC Expander prototype







ORC Pump prototype

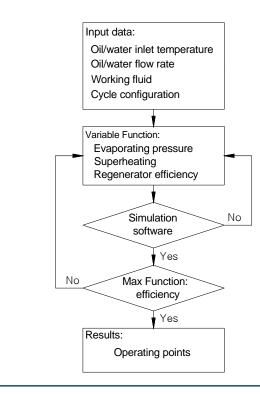


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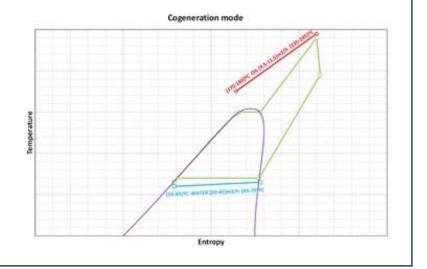
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Simulation software

Using estimated efficiencies for expander and pump, a simulation software has been used to optimize the performance in the desired operating point (considering the regenerative configuration activated up to 250°C and producing hot water between 60 and 80°C).



Evaporating pressure, the superheating and the regenerator efficiency have been optimized in order to reach the maximum efficiency.



Rank[®]



ORC scaled prototype

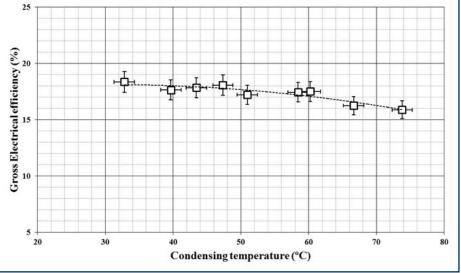
On the other hand, an ORC scaled prototype (1:3) has been constructed to optimize the design. In this way, the experimental results are used to feedback the optimization software and tune the final design.

Finally, the expander prototype has been designed according to a high efficiency system in cogeneration mode

Expander Prototype (T_{max}=240-250°C)



+ + + +





ORC scaled prototype

With the final designs of the components, a test accumulating operating hours is carried out.

- Good performance results are obtained
- Degradation has been observed









ORC prototypes

Three CHP prototypes have been constructed, tested and optimized (control parameters adjusted), and finally installed in the demo sites (2 units in Turkey and 1 unit in Belgium)













	DESIGN	OPTIMIZAT			GRATION	
	ORC	prototype	25			
Rank.			Partial			
			Test 1	Test 2	Test 3	Test 4
	Thermal oil inlet temper	ature (°C)	206	217	203	210
			10.0			
	Thermal oil outlet tempe		133	155	143	143
	Thermal oil flow rate (m	³/h)	10	10	143 12	
	Thermal oil flow rate (m Thermal oil thermal pow	³ /h) ver (kWt)		10 380		143
	Thermal oil flow rate (m Thermal oil thermal pow Water inlet temperature	³ /h) ver (kWt) (°C)	10	10	12	143 10
	Thermal oil flow rate (m Thermal oil thermal pow	³ /h) ver (kWt) (°C)	10 410	10 380	12 415	143 10 408
	Thermal oil flow rate (m Thermal oil thermal pow Water inlet temperature	³ /h) ver (kWt) (°C)	10 410 36	10 380 38	12 415 58	143 10 408 55
	Thermal oil flow rate (m Thermal oil thermal pow Water inlet temperature Water outlet temperature	³ /h) /er (kWt) (°C) /e (°C)	10 410 36 46	10 380 38 48	12 415 58 68	143 10 408 55 65
	Thermal oil flow rate (m Thermal oil thermal pow Water inlet temperature Water outlet temperature Water flow rate (m ³ /h)	³ /h) /er (kWt) (°C) /e (°C) Wt)	10 410 36 46 28	10 380 38 48 28	12 415 58 68 27	143 10 408 55 65 29
	Thermal oil flow rate (m Thermal oil thermal pow Water inlet temperature Water outlet temperature Water flow rate (m ³ /h) Water thermal power (k	³ /h) /er (kWt) (°C) /re (°C) /Vt) :We)	10 410 36 46 28 317	10 380 38 48 28 290	12 415 58 68 27 330	143 10 408 55 65 29 320



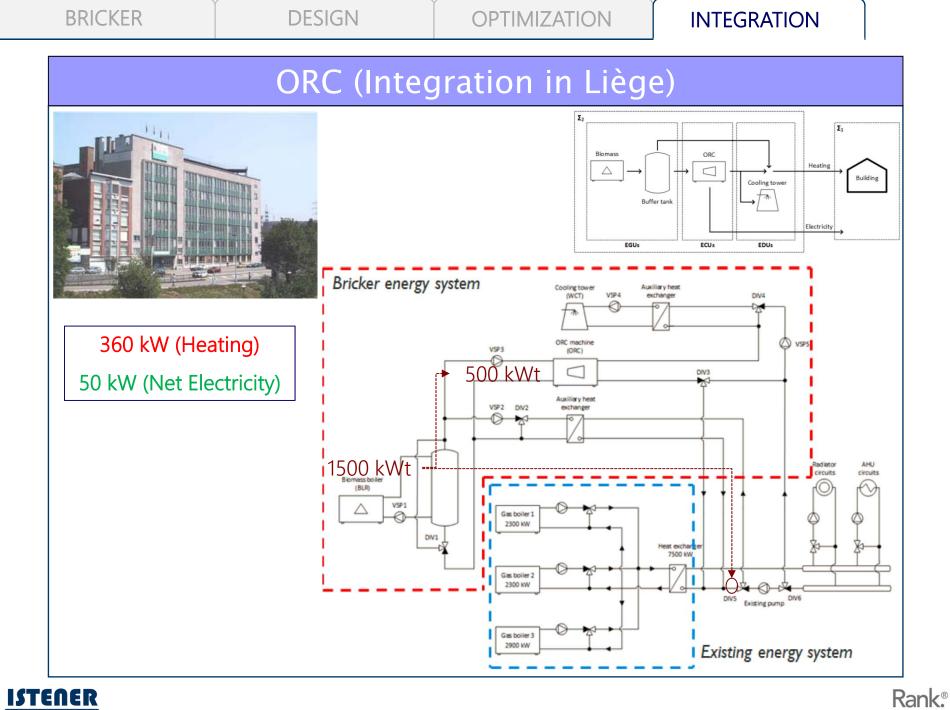
ORC prototypes

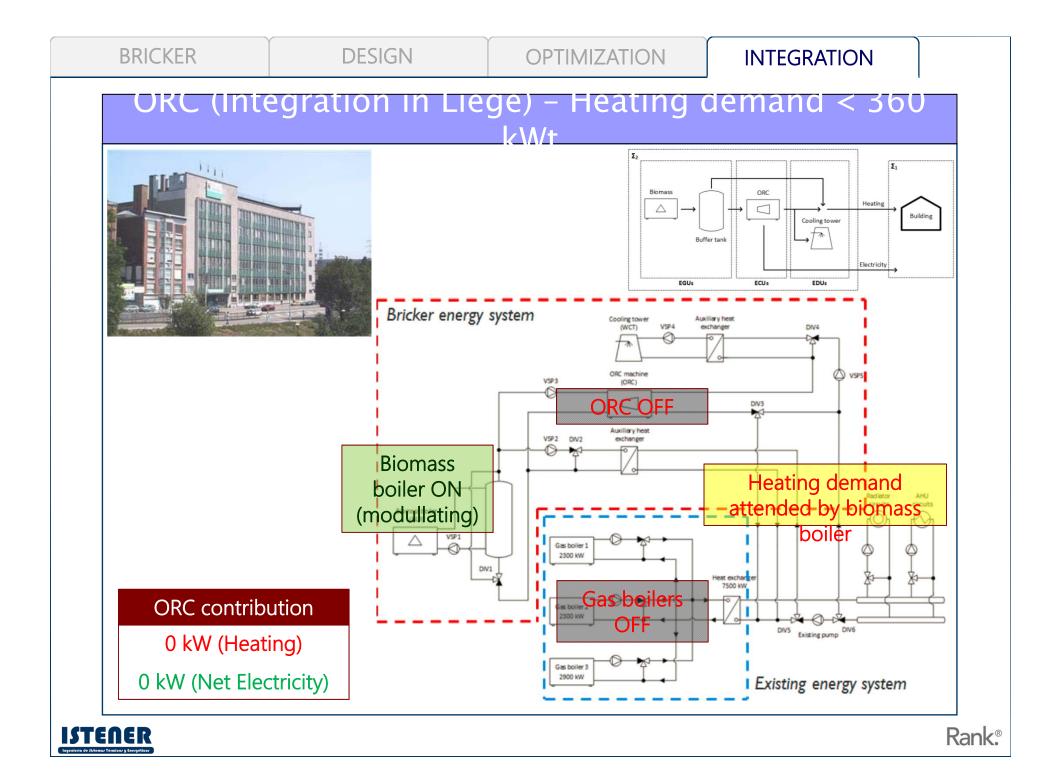
	Expected per	ormance
Rank?	Globa 85%	efficiency
	Generation mode	Cogeneration mode
Thermal oil inlet temperature (°C)	225	225
Thermal oil outlet temperature (°C)	130	150
Thermal oil flow rate (m ³ /h)	9-11	9-11
Thermal oil thermal power (kWt)	525	435
Water inlet temperature (°C)	20	60
Water outlet temperature (°C)	32	70
Water flow rate (m ³ /h)	27-31	27-31
Water thermal power (kWt)	405	345
Gross electrical power (kWe)	85	57
Gross electrical efficiency (%)	>16%	>13%
Net electrical efficiency (%)	14,50%	11,50%

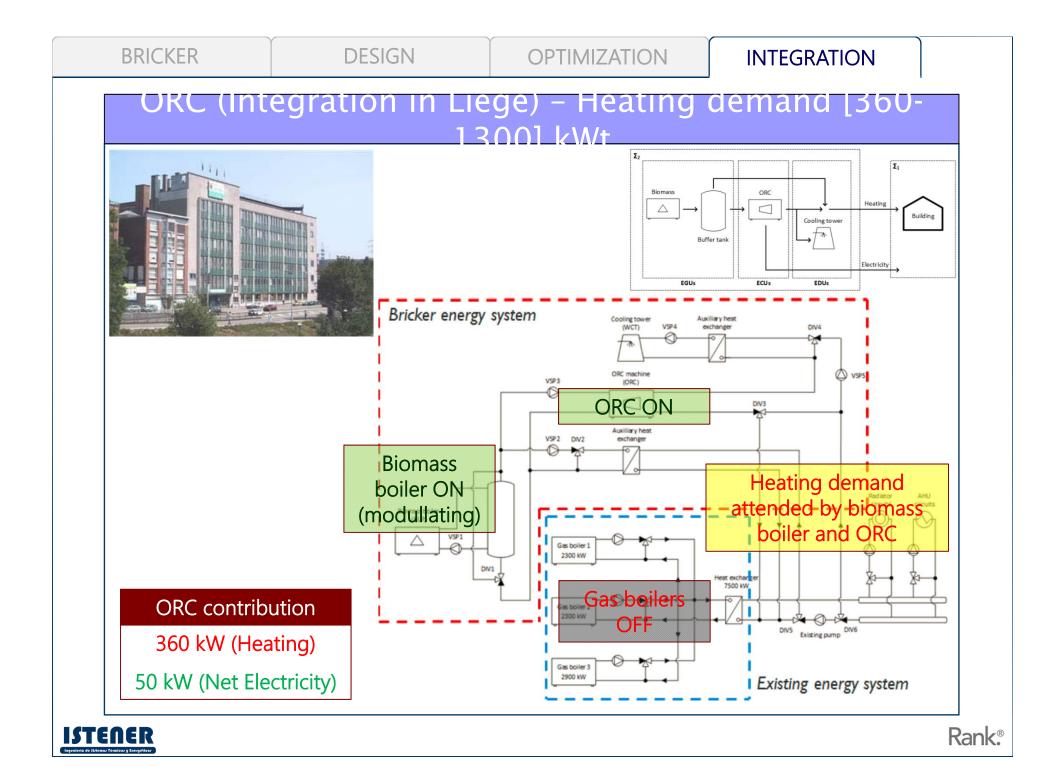


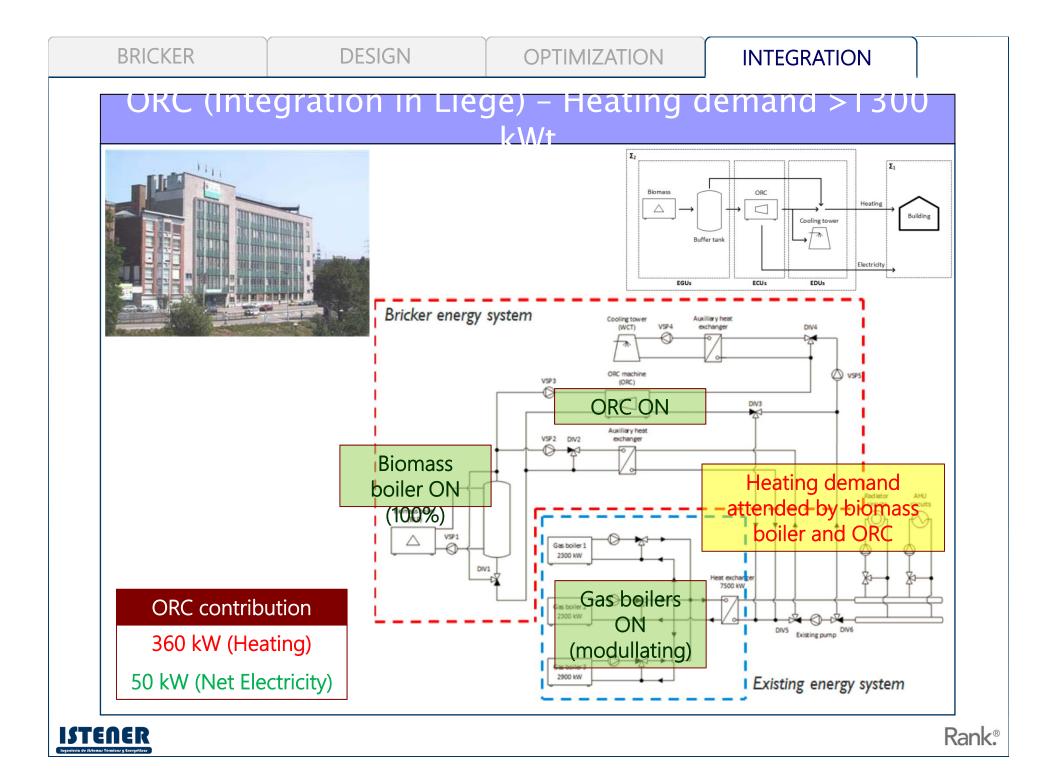
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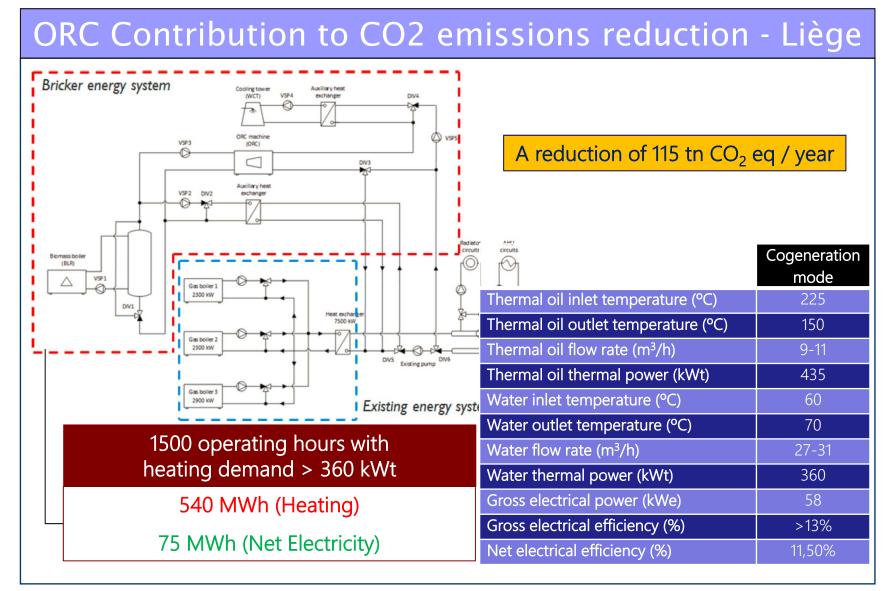








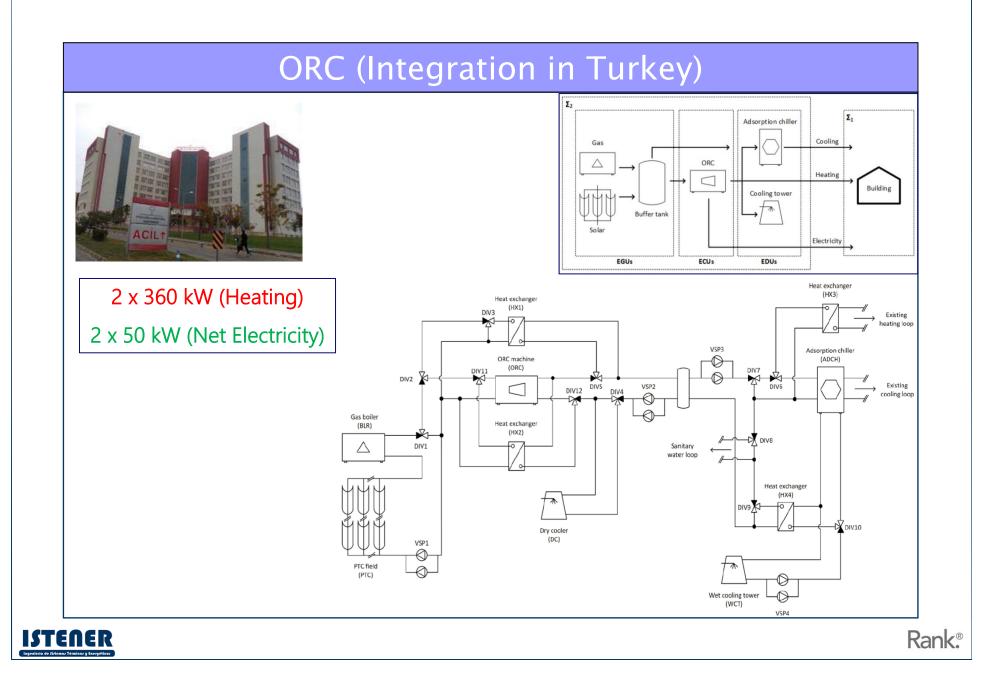


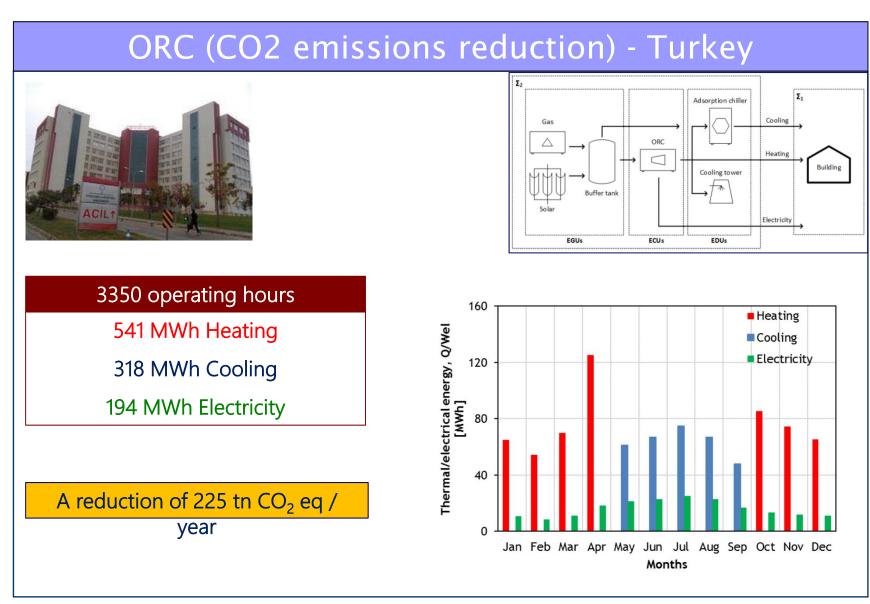




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INTEGRATION







Commercial product (Rank[®] HTC)

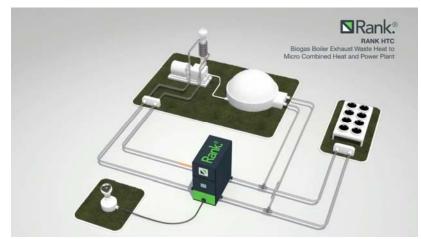
Only cogeneration mode makes sense attending global efficiencies

- Up to 80°C is a general demand in buildings
- Activation limited up to 210°C
- Global efficiency [(H+E)/Q] up to 85%

Product	Model	HTC1	HTC2	HTC3
	Fluid	Thermal oil	Thermal oil	Thermal oil
Heat agurag	Flow rate (m ³ /h)	12,5	27,0	44,0
Heat source	Inlet temperature (°C)	180-210	180-210	180-210
	Thermal power (kWt)	325-470	690-995	1135-1585
	Fluid	Water	Water	Water
	Flow rate (m ³ /h)	19,0	40,0	65,5
Heat sink	Inlet temperature (°C)	45-65	45-65	45-65
	Outlet temperature (°C)	60-80	60-80	60-80
	Thermal power (kWt)	245-330	515-700	845-1150
Electrical power	Gross power (kWe)	27-43	58-91	95-143

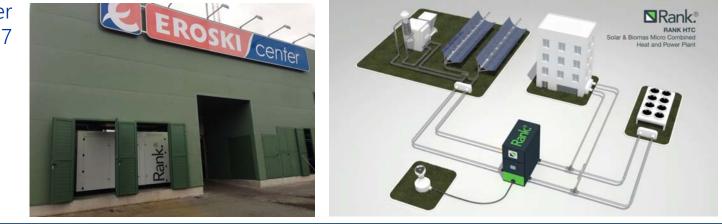


Commercial product (Rank® HTC)





September 2017









THANKS...

Any Question?

Prof. Joaquín Navarro Esbrí ISTENER Research Group Director Rank® founding partner