

# Combined Heat and Power Plants - Sizing and Integration

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Back to basics

Performance of CHP Plants

Different Types of CHP Plants

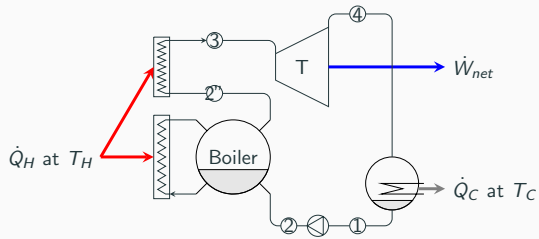
Economical Evaluation of Combined Heat and Power

Example Case Study

## Back to basics

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# Heat to Work Conversion Efficiency



**Figure 1** – Backpressure turbine

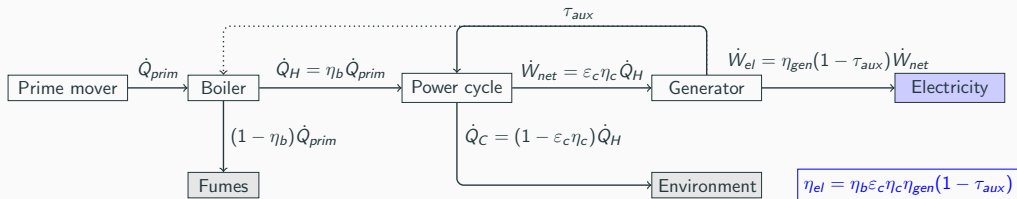
Applying the first and second principles of Thermodynamic leads to :

$$\begin{cases} \dot{W}_{net} = \varepsilon_c \eta_c \dot{Q}_H \\ \dot{Q}_C = \dot{Q}_H - \dot{W}_{net} \end{cases}$$

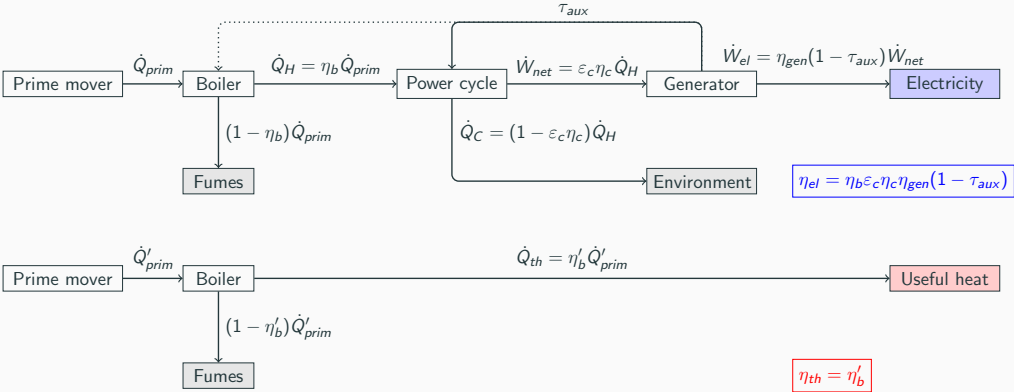
Where

$$\eta_c = 1 - \frac{T_C}{T_H}$$
$$\varepsilon_c = 50 \% \dots 75 \%$$

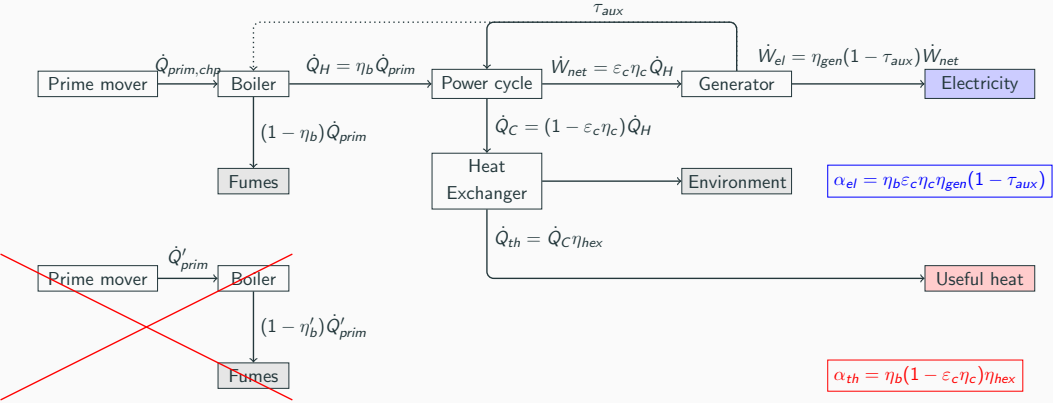
# Energy Balance



# Energy Balance



# Energy Balance



# Performance of CHP Plants

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Based on energy

$$\left\{ \begin{array}{l} \alpha_{el} = \frac{\dot{W}_{el}}{\dot{Q}_{prim,chp}} = \eta_b(1 - \varepsilon_c \eta_c) \eta_{hex} \\ \alpha_{th} = \frac{\dot{Q}_{th}}{\dot{Q}_{prim,chp}} = \eta_b(1 - \varepsilon_c \eta_c) \eta_{hex} \end{array} \right. \rightarrow \eta_{chp} = \alpha_{el} + \alpha_{th}$$

Based on exergy where  $T_{th}$  is the temperature of the useful heat.

$$\eta_{ex,chp} = \frac{\dot{W}_{el} + \dot{Q}_{th} \left(1 - \frac{T_0}{T_{th}}\right)}{\dot{m}_c e_c} = \frac{\alpha_{el}}{f} \left[1 + \phi \left(1 - \frac{T_0}{T_{th}}\right)\right]$$

# Primary Energy Saving

**For separate production :**  $\dot{Q}_{prim,sep} = \frac{\dot{W}_{el}}{\eta_{el}} + \frac{\dot{Q}_{th}}{\eta_{th}}$

**For combined generation :**  $\dot{Q}_{prim,chp} = \frac{\dot{W}_{el}}{\alpha_{el}} + \frac{\dot{Q}_{th}}{\alpha_{th}}$

The primary energy saving is thus :

$$PES \triangleq \frac{\dot{Q}_{prim,sep} - \dot{Q}_{prim,chp}}{\dot{Q}_{prim,sep}} = 1 - \frac{1}{\frac{\alpha_{el}}{\eta_{el}} + \frac{\alpha_{th}}{\eta_{th}}}$$

## **Different Types of CHP Plants**

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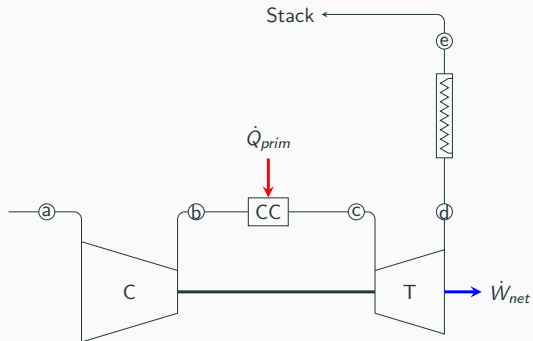


Figure 3 – Gas Turbine

$$\alpha_{el} \simeq 30\%$$

$$\alpha_{th} \simeq 55\%$$

$$\eta_{chp} \simeq 85\%$$

$$\eta_{ex,chp} = 55\%$$

$$PES \simeq 10\%$$

# Combined cycles

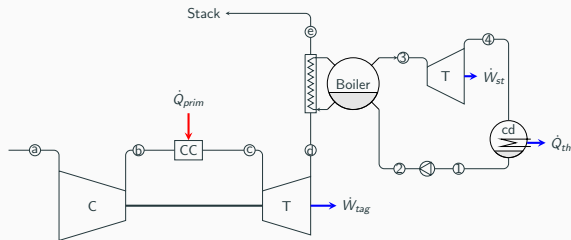


Figure 4 – Combined Cycle

$$\alpha_{el} \simeq 35 \%$$

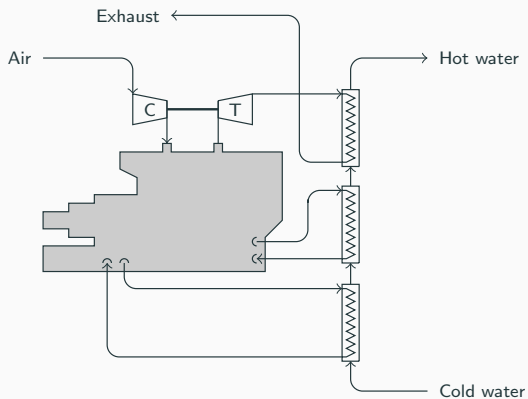
$$\alpha_{th} \simeq 50 \%$$

$$\eta_{chp} \simeq 85 \%$$

$$\eta_{ex, chp} \simeq 45 \%$$

$$PES \simeq 15 \%$$

# Internal Combustion Engine



$$\alpha_{el} \simeq 40\%$$

$$\alpha_{th} \simeq 46\%$$

$$\eta_{chp} \simeq 86\%$$

$$\eta_{ex,chp} \simeq 48\%$$

$$PES \simeq 20\%$$

**Figure 5** – Internal combustion engines

# **Economical Evaluation of Combined Heat and Power**

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# The Net Present Value

## Definition

The excess of the present value (PV) of cash inflows generated by the project over the amount of the initial investment  $C_0$ .

$$NPV = PV - C_0 = \sum_{k=1}^N A_k(1 + d)^{-k} - C$$

For constant cash inflows,  $NPV = A/\psi - C$  where  $\psi = \frac{d}{1 - (1 + d)^{-N}}$ .

## Decision rule

If NPV is positive, accept the project. Otherwise, reject it.

## Estimating the Installation Cost

### The rule of “six tenths”

As size increases, cost increases by an exponent of six-tenths.

$$C = C_{ref} \left( \frac{P_{rated}}{P_{rated,ref}} \right)^{0.6}$$

- Generally speaking, costs are increasing with an exponent  $a$  whose value is between 0.3 (building, civil works) to 1.0 (scale-up by installation of multiple units).
- Inflation  $\lambda$  can influence the reference cost  $C_{ref}$  according to  $C_{ref,N} = C_{ref,0}(1 + \lambda)^N$ .
- For developing technologies, reference costs may decrease due to increasing production volumes.

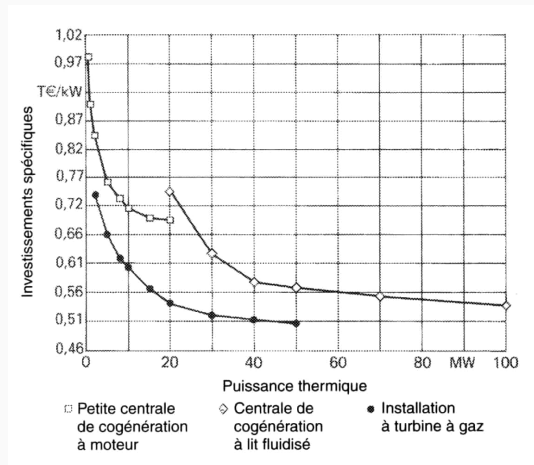


Figure 6 – Coûts spécifiques de différentes installations

## Levelized Cost of Energy (LCOE)

For constant equivalent utilisation time and constant conversion efficiency over the project lifetime, the total system cost is :

$$\begin{aligned} TSC &= \sum_{k=1}^N \left[ C\psi(1+d)^{-k} + \left( \frac{P_{rated}\tau_e C_f}{\eta} + U_{fix} + u_{var}P_{rated}\tau_e \right) (1+d)^{-k} \right] \\ &= \frac{P_{rated}\tau_e}{\psi} \left( \frac{C\psi}{P_{rated}\tau_e} + \frac{C_f}{\eta} + \frac{U_{fix}}{P_{rated}\tau_e} + u_{var} \right) \end{aligned}$$

$$LCOE = \frac{TSC}{\frac{P_{rated}\tau_e}{\psi}} = \underbrace{\frac{C\psi}{P_{rated}\tau_e}}_{\text{CAPEX}} + \underbrace{\frac{U_{fix}}{P_{rated}\tau_e} + \frac{C_f}{\eta} + u_{var}}_{\text{OPEX}} + \underbrace{\frac{C_f}{\eta} + u_{var}}_{\text{marginal cost}}$$

## Evaluating the Cost of Heat

- Electricity is already available at low cost (without tax!!) from the grid while there is no global market for heat.
- Heat is difficult to transport.

Heat is the main product and electricity is the by-product !

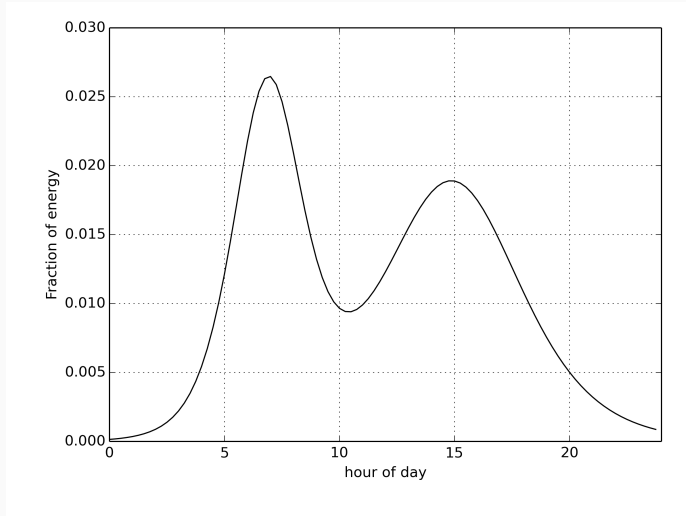
$$COH = \underbrace{\frac{C\psi}{P_{th,rated}\tau_e}}_{\text{CAPEX}} + \underbrace{\frac{U_{fix}}{P_{th,rated}\tau_e} + \frac{C_f}{\eta} + u_{var} - (Y_{el} + \tau_{cv} Y_{cv}) \frac{\alpha_{el}}{\alpha_{th}}}_{\text{OPEX}}$$

marginal cost

## Example Case Study

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# Energy Integration of a CHP Plant



**Figure 7** – Non-dimensional heat consumption profile (Sart-Tilman Campus)

# Load curve for heat demand

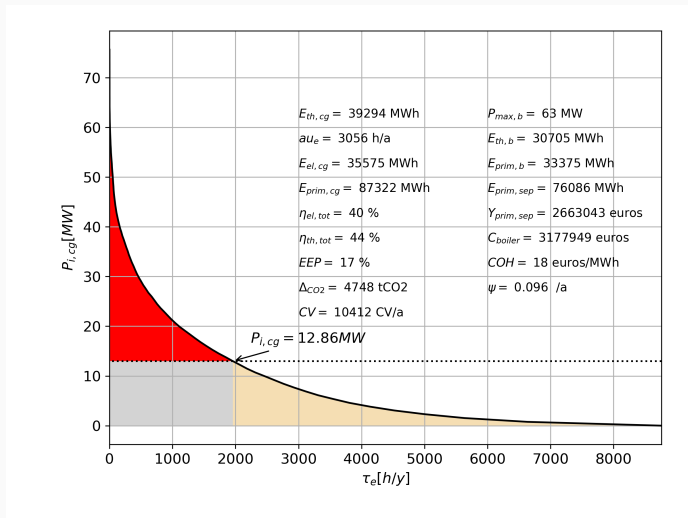


Figure 8 – Cumulative heat load for Sart-Tilman campus (total of 70 000 MWh/y).



# Optimizing the Size of a CHP

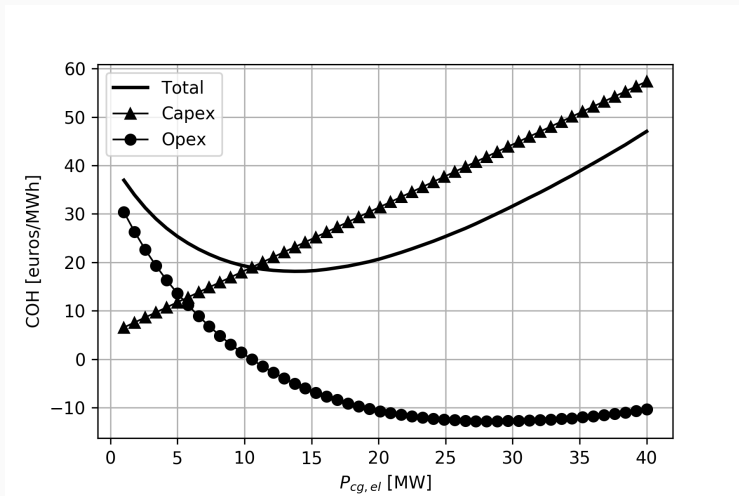


Figure 9 – COH versus CHP plant size